

In the Specification:

Please amend the specification as follows:

Page 1, paragraph 1:

Field of the Invention

The invention relates to a method and an apparatus for processing flue gas scrubber material flows ~~according to the preamble of claim 1. The invention also relates to an apparatus for carrying out the method according to the preamble of claim 9.~~

Background of the Invention

Page 2, first full paragraph:

Summary of the Invention

It is an aim of the invention to eliminate the above-mentioned drawbacks and to present a method, wherein it is possible to control foaming without specific anti-foam chemicals.—To attain this purpose, ~~the method according to the invention is primarily characterized in what will be presented in the characterizing part of the appended claim 1.~~

Page 3, first paragraph:

Brief Description of the Drawings

In the following, the invention will be described in more detail with reference to the appended drawings, in which

Page 3, second paragraph:

Detailed Description of the Invention

Fig. 1 shows the desulphurization plant for flue gases in a diesel power plant as a general process chart, which plant includes a gas scrubber 1, whose operating principle is known, to which the flue gases created in fuel combustion are directed from the diesel motors (arrow A) and from which the cleaned flue gases are directed away via a waste flue (arrow B). Here the gas scrubber 1 refers to an actual scrubber tower, where flue gases and washing fluid are put into contact with each other and in whose lower part the washing fluid accumulates. Gas scrubber 1 is a limestone-based scrubber. From limestone silo 2, limestone is supplied in a powdered form to the limestone slurry tank 3, from where it is pumped into the scrubber 1. Limestone slurry is recycled from the lower part of the scrubber 1 to nozzles 4, which are located above the inlet of flue gases and which form a spray zone, which scrubs the flue gases with a countercurrent principle. Calcium carbonate reacts with the sulphur compounds of flue gases by forming calcium sulphite, which oxidizes into calcium sulphate i. e. gypsum because of the oxygen

coming in with flue gases and the forced oxidation taking place in the lower part of the scrubber. Oxidation air is supplied to the fluid volume in the lower part of the scrubber via line C. There is also a mixer in the lower part of the scrubber, the purpose of which is to mix oxidation air to the fluid volume. Gypsum slurry is formed on the bottom of the gas scrubber 1, which slurry is directed from the bottom of the scrubber via the waste line D to the separator 5. The separator is a hydrocyclone, whose substantially gypsum-free excess is directed back to the scrubber 1 via the recovery line E as washing fluid. Water is used as the carrier of the washing fluid, which water carries the materials used in the flue gas scrubbing process and formed in it. The waste line D and the recovery line E form a recycle line, the purpose of which is to create a water circulation as closed as possible in order to keep the need for fresh water as small as possible. The reject of the hydrocyclone, which is gypsum slurry, which has a high solid matter content, is directed to the belt filter 6, where water is further removed from the gypsum by filtering and from on top of which the gypsum cake is moved to further processing. The washing fluid received as filtrate from the belt filter can be further recycled to the scrubber 1.